

# Acquisition and Analysis of Data in a Pressurized Entrained-Flow Coal Gasifier for the Purposes of Simulation Validation

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# Outline

- Introduction
- Background – coal gasification research
- U. Utah pilot-scale coal gasifier
- Types of data available for validation
- Performance issues
- Uncertainty considerations
- Conclusions



# Introduction

- Industrial-scale coal gasifiers are primarily pressurized, O<sub>2</sub>-blown, entrained-flow variety
- Cost of gasification systems provides strong incentive to optimize using computational simulation
- Access to gasifiers for acquisition of validation data is challenging





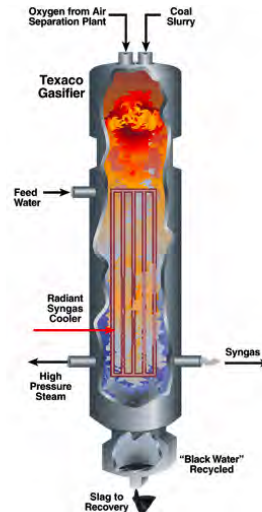
# Pressurized O<sub>2</sub>-Blown Entrained-Flow Gasifiers

Downflow

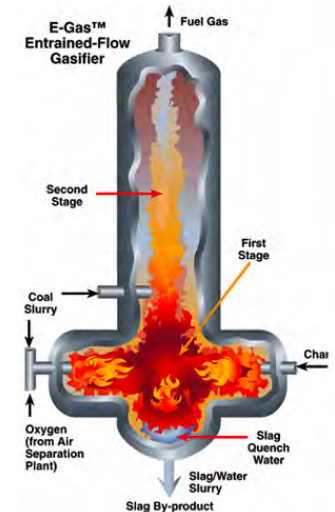
Upflow

Refractory-Lined

GE Energy

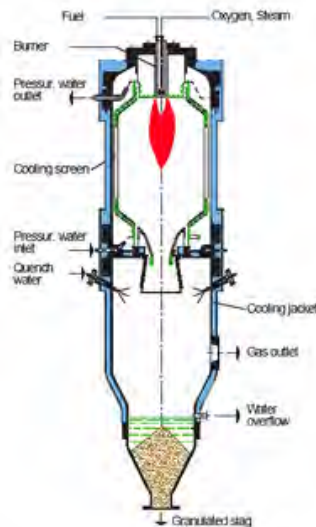


ConocoPhillips

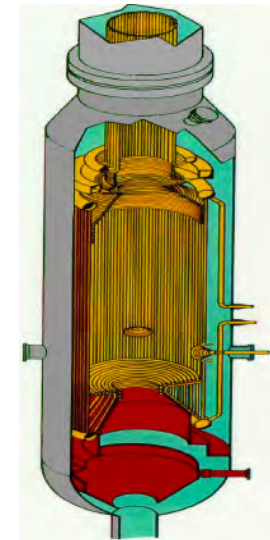


Membrane Wall

SIEMENS



Shell Global  
Solutions

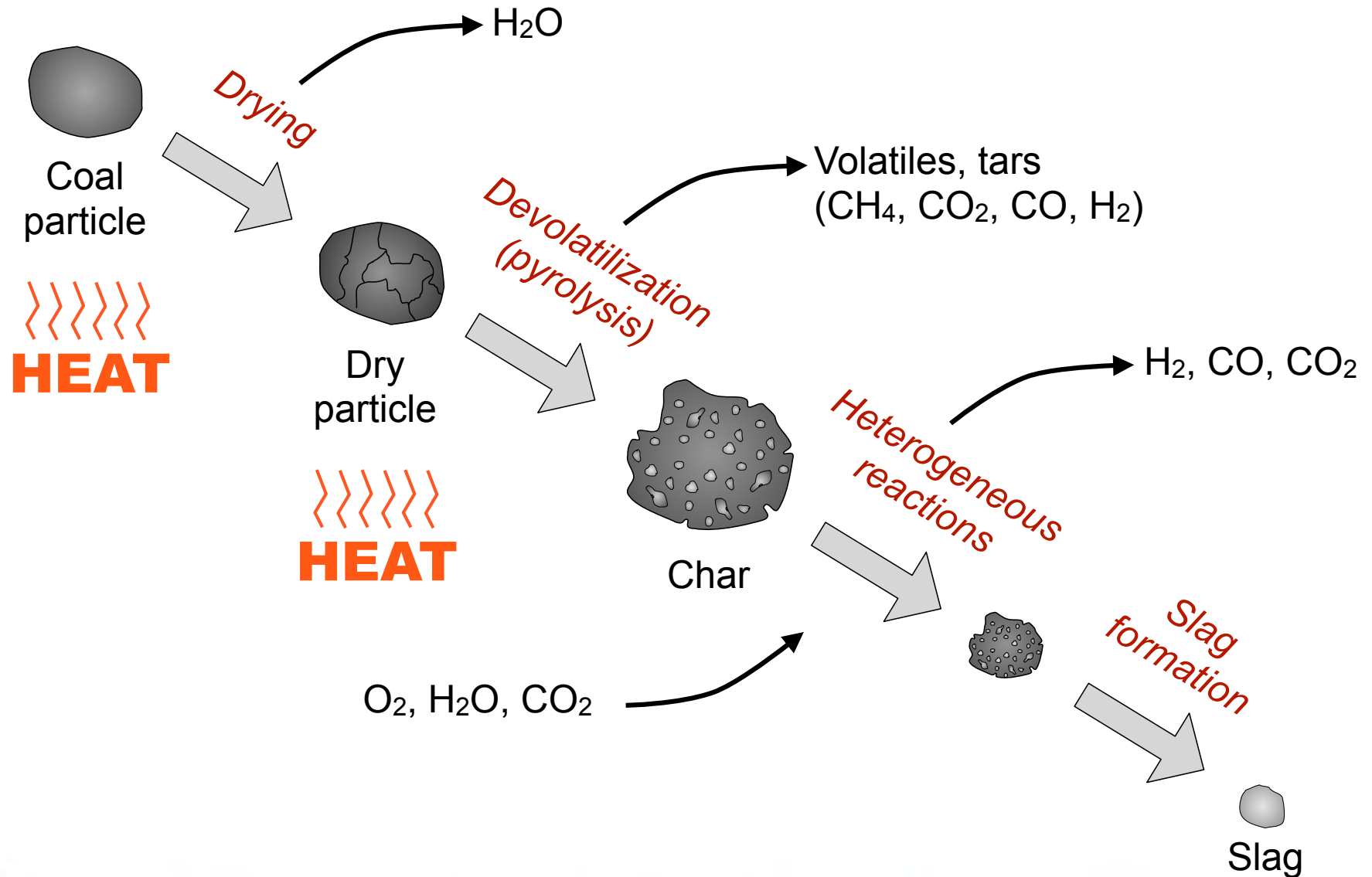


# Challenges of Validation Data Acquisition

- High temperature
  - 1300-1500°C at reactor exit
  - In excess of 2000°C within oxy-coal flame
- High pressure
  - IGCC application typically 25-30 atm (400 psi)
  - Chemicals / fuel production 70+ atm (1000+ psi)
- Corrosive environment
  - Reducing environment
  - Gaseous sulfur species ( $\text{H}_2\text{S}$ , COS)
  - Molten coal slag
- Consequences
  - Crossing pressure boundary for gas sampling creates safety concerns
  - Thermocouples typically last only a few days

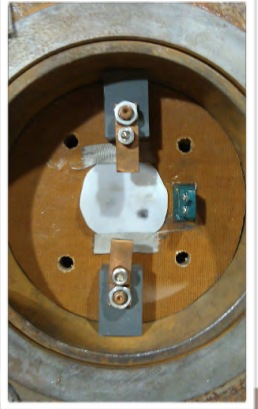


# Fundamental Coal Gasification Studies



# Experimental Evaluation of Coal Conversion

- Drop tube (entrained-flow) furnaces
  - Pyrolysis yields
  - Char gasification kinetics
  - Physical transformations of coal particles
- Wire mesh heaters
  - Pyrolysis yields
- Thermogravimetric analyzers (TGAs)
  - Heterogeneous char gasification kinetics
- Mini-gasifiers
  - Electrically heated
  - Gases ( $\text{CO}_2$ ,  $\text{O}_2$ ) supplied from laboratory cylinders



# “Small” versus “Big”

- Fundamental Studies (“small”)
  - Up to perhaps 2 kg/day in entrained-flow reactors
  - Bottled gases
  - Electrically heated
- Commercial-Scale Systems (“big”)
  - Hundreds of tons of coal (petcoke) per day
  - Oxygen-blown, with all associated mess
  - Difficult to access
- Need “medium” scale system to bridge this gap of 5 orders of magnitude





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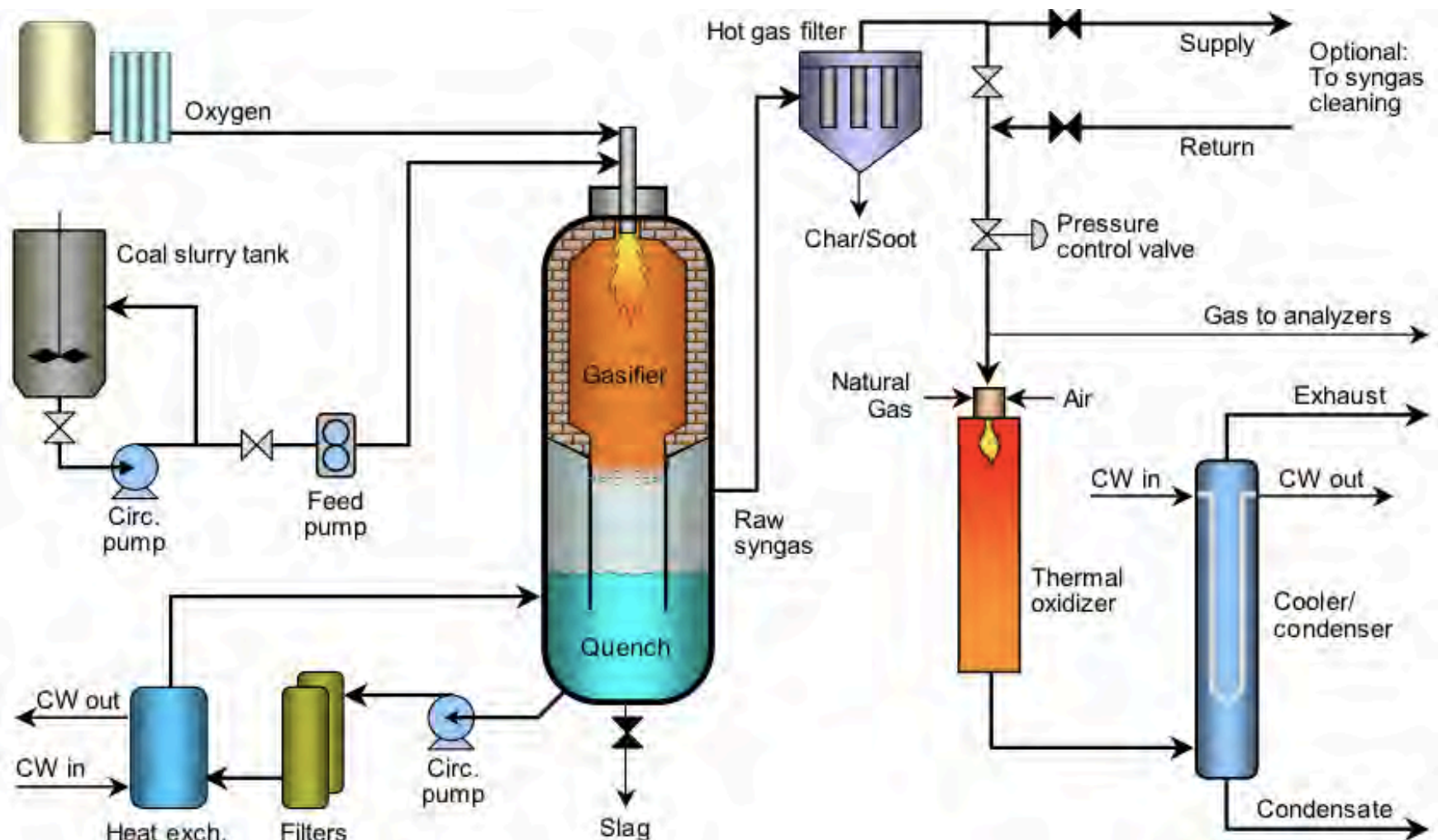


# Bridging the Gap: UofU Gasifier

- Designed to operate like a “large” system
  - No electrical heating
  - Only inputs are oxygen and coal (slurry)
  - Similar in design to a GE gasifier
- Accessible like a “small” system
  - Reactor “stretched out” to decrease diameter and allow sampling at multiple residence times
  - Several (six) sampling ports down length of reactor
  - Six thermocouples for temperature measurement

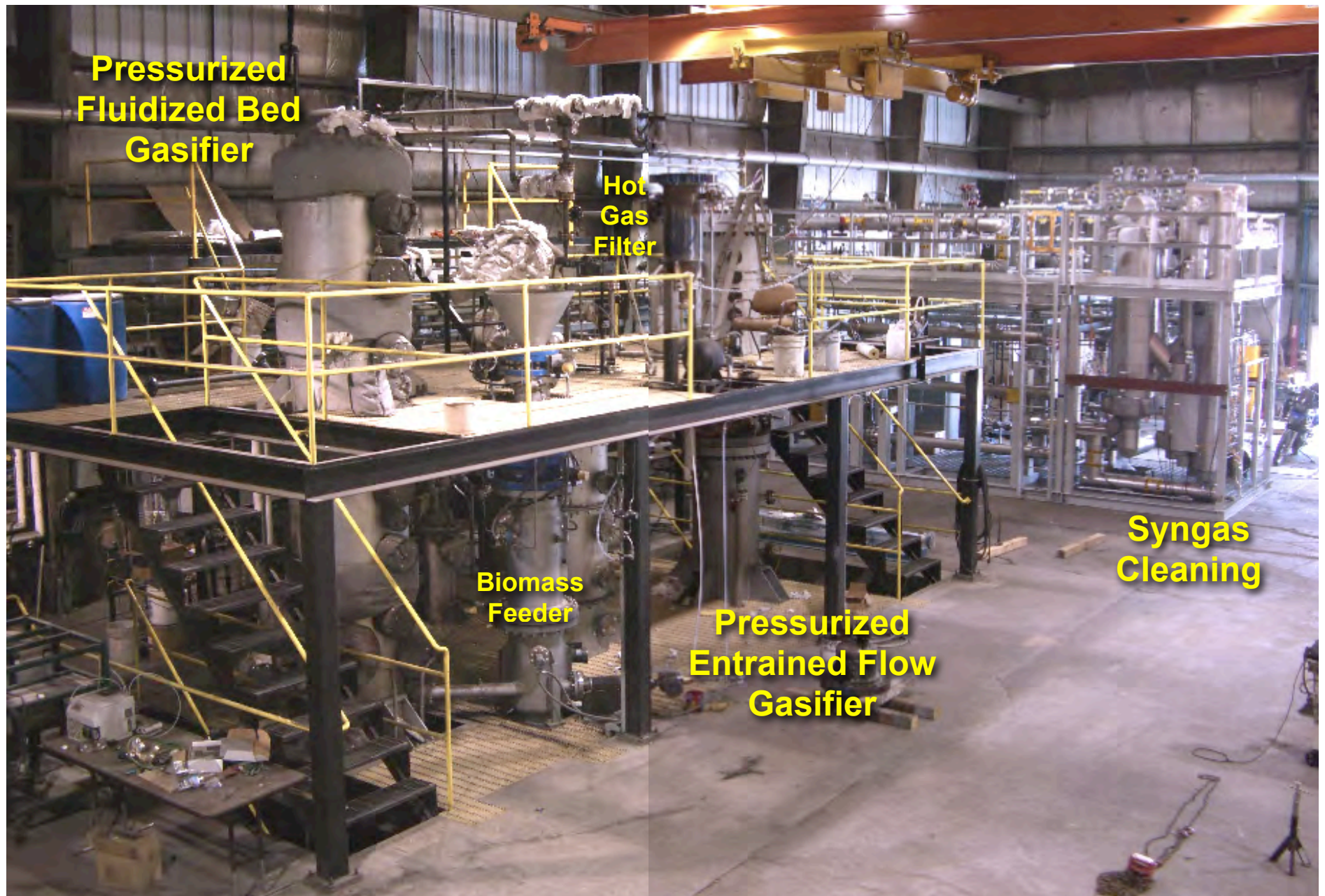


# Gasifier System Schematic





# Gasification Research Laboratory





# Entrained-Flow Gasifier



# Oxygen Supply System

- On-site oxygen tank
  - 6,000 gallons / 20 tons
  - Serves gasification and oxy-fuel systems
- “Trifecta” system to boost pressure
  - 325 psi
  - Limits standard operation pressure to ca. 260 psi
  - Higher pressures require auxiliary high pressure supply
- Flow control system to gasifier
  - Pressure regulator
  - Control valve
  - Coriolis flowmeter





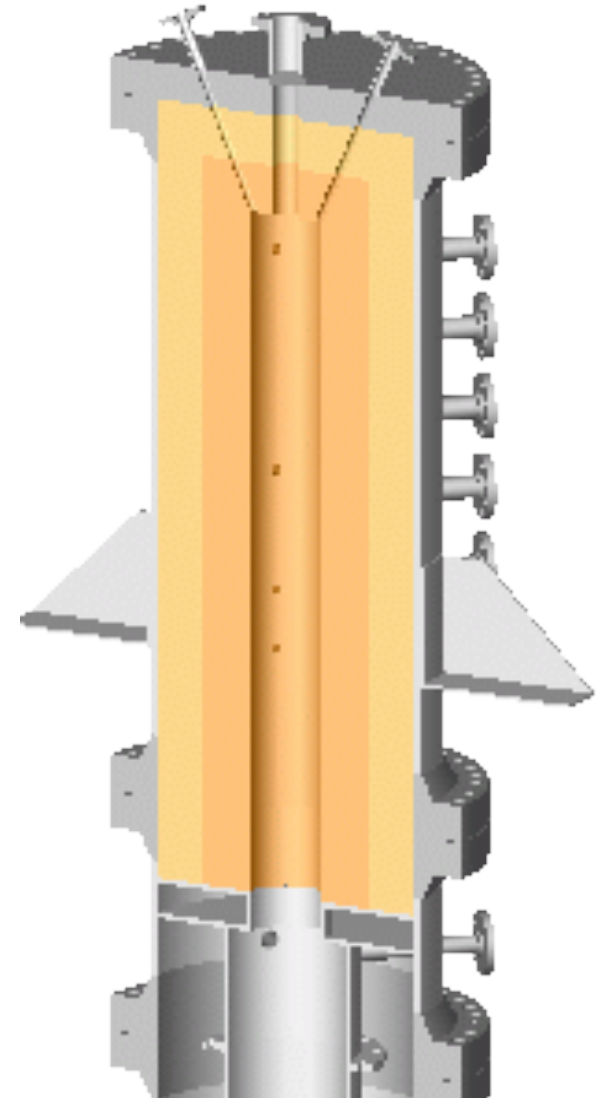
# Gasifier Specifications

Parameter	Typical	Max.
Pressure (bar)	18	31
Temperature (°C)	1425	1700
Slurry feed rate (lit/h)	50	150
Coal feed rate (kg/h dry)	30	80
Thermal input (kW <sub>th</sub> )	220	600
Slurry concentration (wt%)	59	65
Oxygen feed rate (kg/h)	35	150
Syngas production (m <sup>3</sup> /h dry)	50	150



# Reactor Details

- Reactor dimensions
  - 30 inch (0.75 m) pressure vessel
  - 8.5 inch (0.22 m) reactor ID
  - 60 inch (1.5 m) reactor length
  - Designed to identify development of gas and condensed phases as coal undergoes conversion
- Sample ports
  - Twelve opposing 2 inch (5 cm) ports at six levels for sampling, optical diagnostics
  - Two additional 2 inch (5 cm) ports at burner level
  - Six 1 inch (2.5 cm) ports for temperature/pressure measurement





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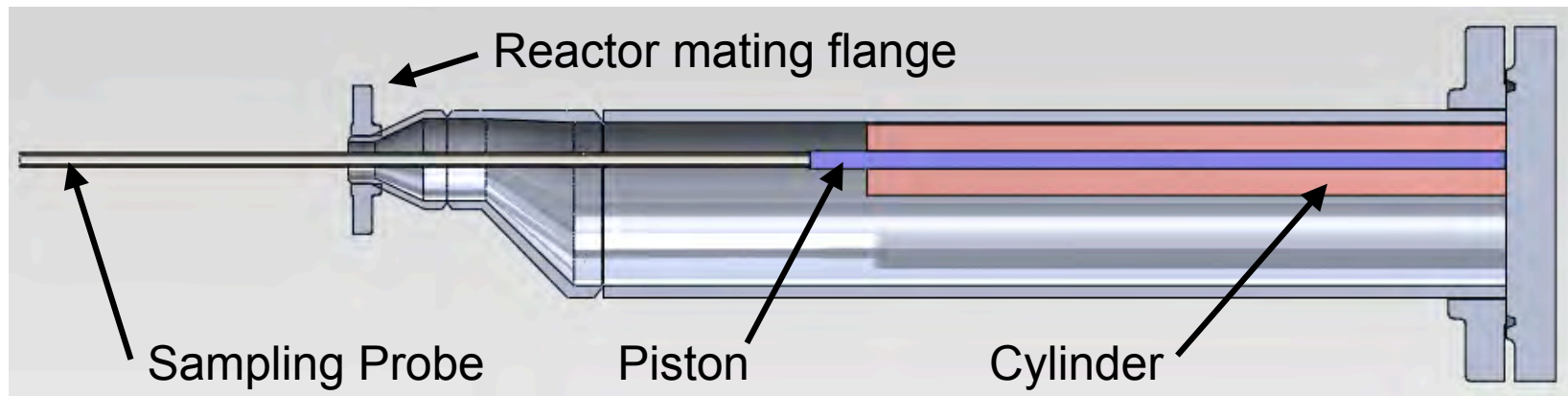
# The Easy Stuff

- Inputs
  - Slurry flow rate and concentration
  - Coal composition
  - Oxygen feed rate
  - Purge flow rates
- Temperatures
  - Five B-type thermocouples along length of reactor
  - Additional thermocouples in quench, on shell, etc.
- Syngas composition
  - Analysis after gas has been quenched, cooled, depressurized
- Solids composition
  - Char caught in filters, slag caught in slag trap
  - Analyzed only after system is depressurized

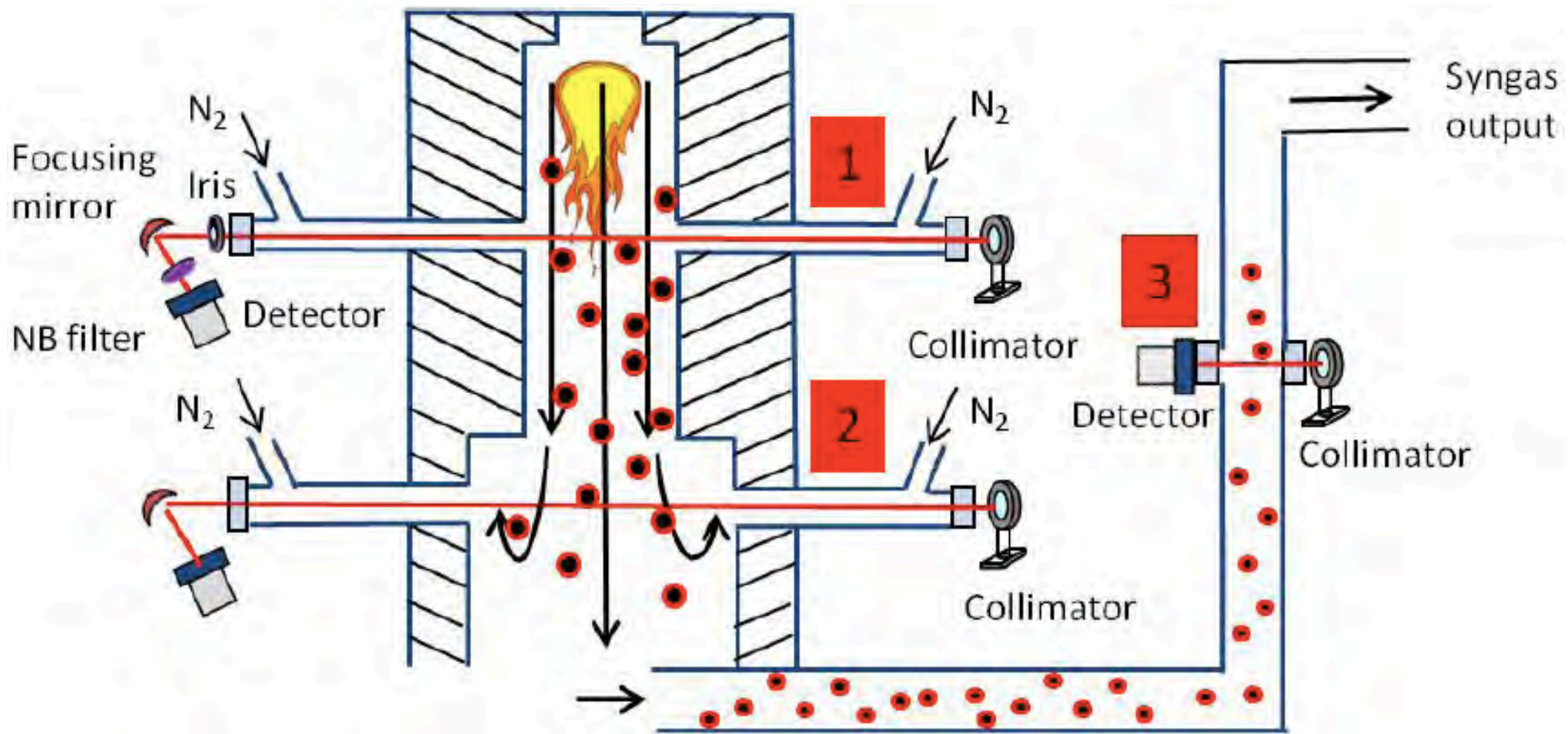


# Extractive Sampling

- Cooled probe for gas sampling within reactor chamber
- Moveable piston will allow quick positioning from wall to centerline of reactor
- Safety systems integrated with gasifier control system
- Can be installed at any of five locations down length of reactor
- Modification of system will allow deposition of condensed-phase material onto probe

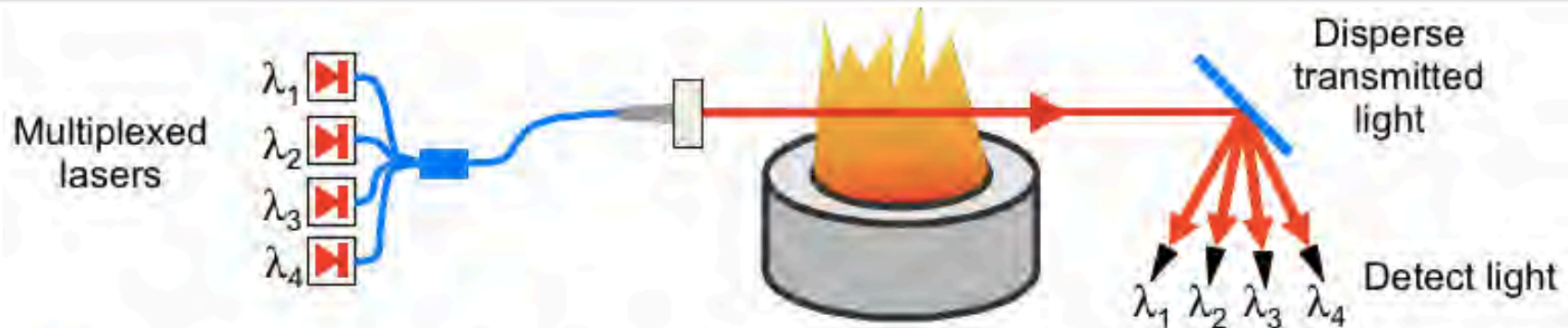


# Measurement Locations for Stanford TDL Sensor Project

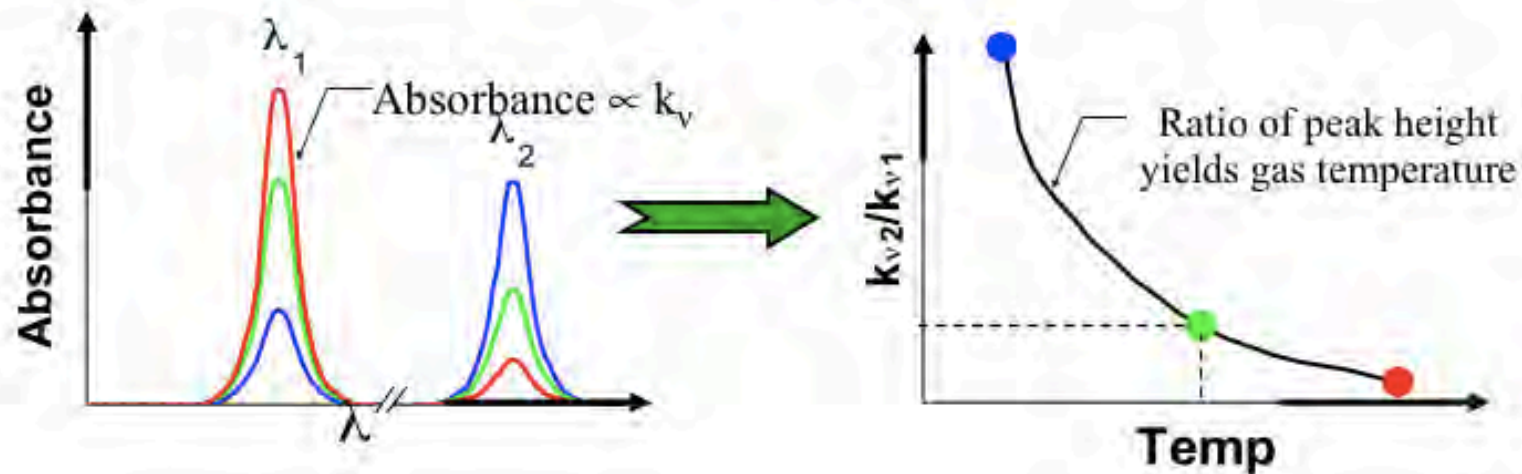




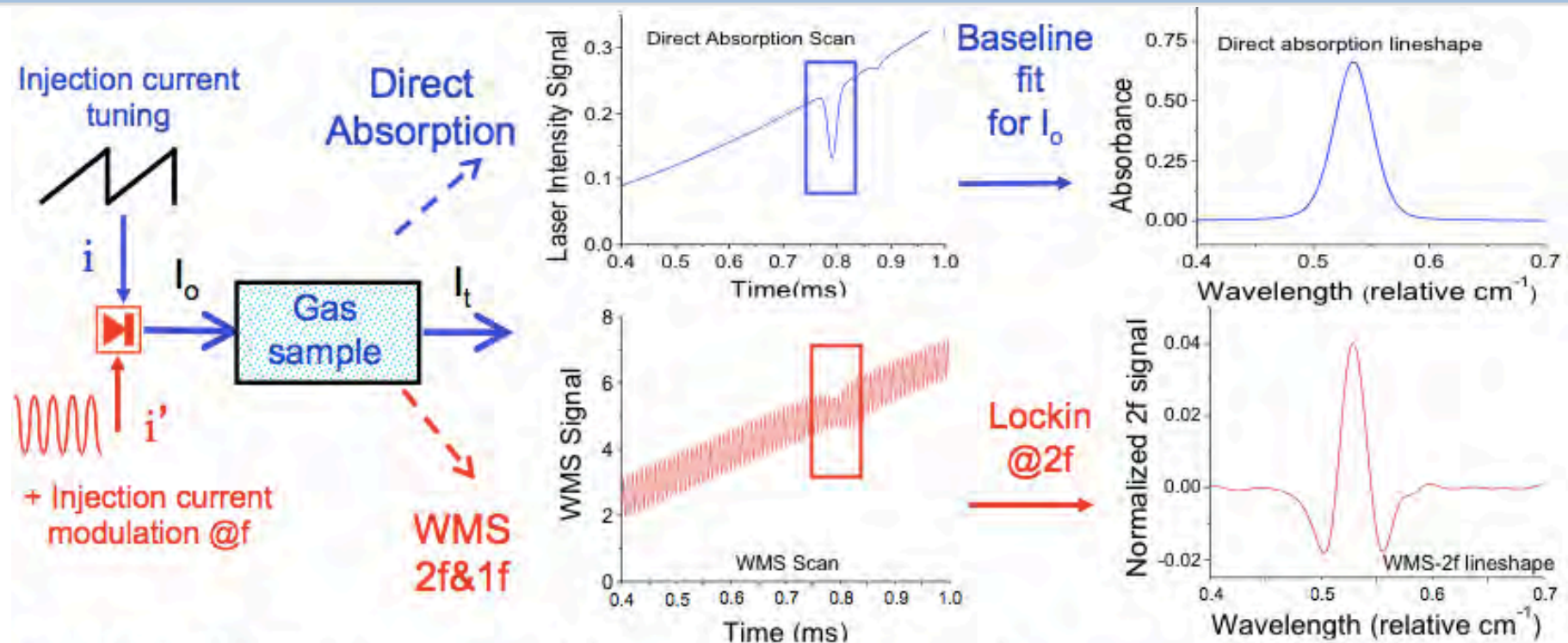
# Absorption Fundamentals: Wavelength-Multiplexed Tunable Diode Laser Sensing



- Absorption of laser light by molecular transitions in the combustion gases
  - Beer's law:  $\text{Transmission} = I/I_0 = e^{-kL}$
  - Absorption coefficient  $k = f(\text{temperature, pressure, gas composition})$
- Ratio of absorbance on two molecular transitions yields gas temperature
- Multiplex additional lasers for more combustion species



# Absorption Fundamentals: Scanned Direct Absorption and Wavelength Modulation Spectroscopy

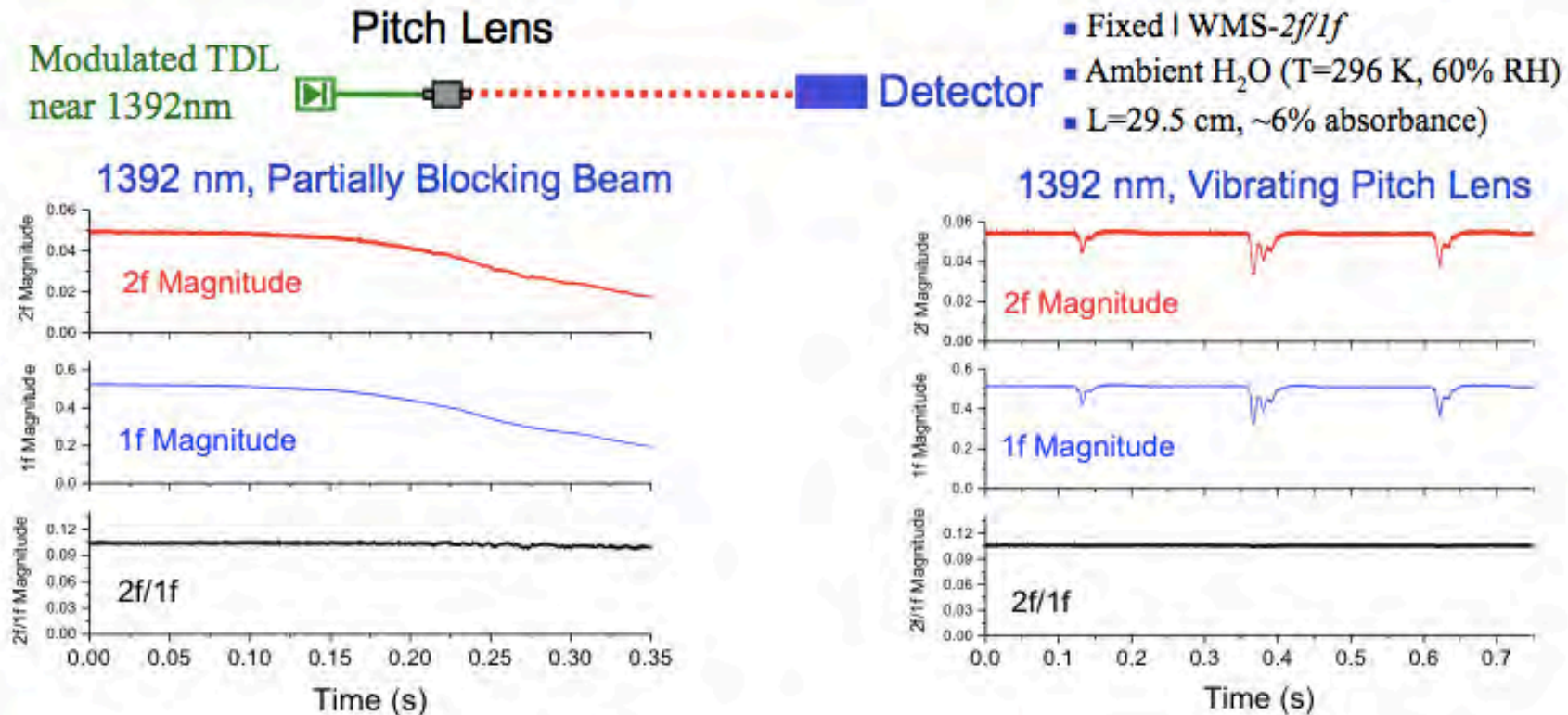


- Direct absorption: Simpler, if absorption is strong enough
- WMS: More sensitive especially for small signals (near zero baseline)
  - Ratio of two WMS-2f signals provides  $T$  (same as direct absorption)
  - WMS with TDLs has improved noise rejection (especially for non-absorption losses)
  - WMS also produces intensity modulation @1f
  - Since both 2f and 1f signals are proportional to  $I$ ; 2f/1f independent of optical losses





# Absorption Fundamentals: Demonstration that Normalization of WMS Improves Signal-to-Noise Ratio

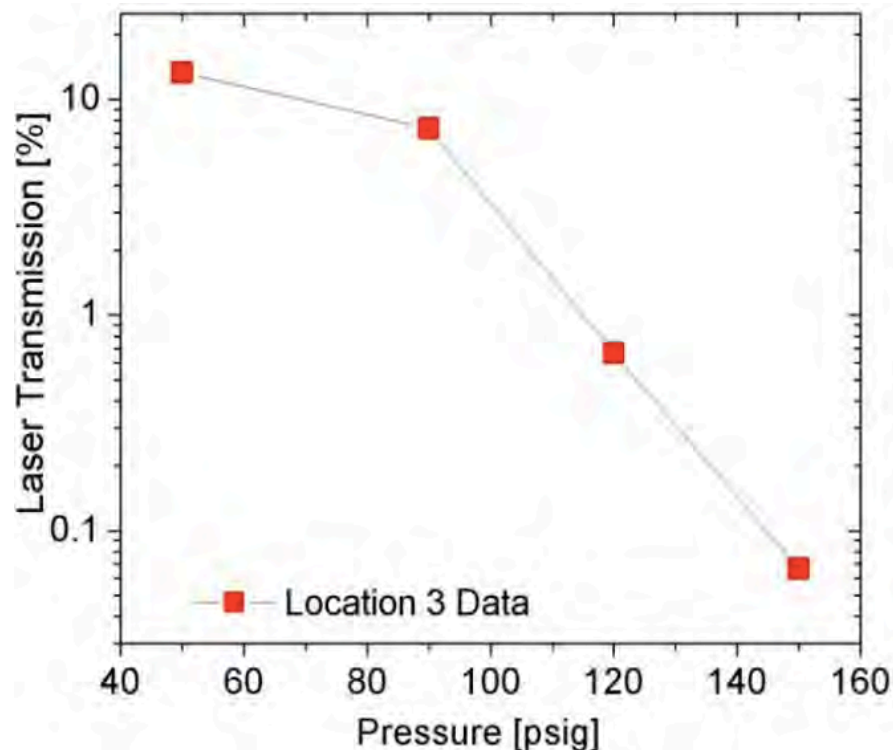


- Demonstrate normalized WMS- $2f/1f$ 
  - No loss of signal when beam attenuated (e.g., scattering losses)
  - No loss of signal when optical alignment is spoiled by vibration
- Normalized WMS- $2f/1f$  signals free from window fouling and particulate loading

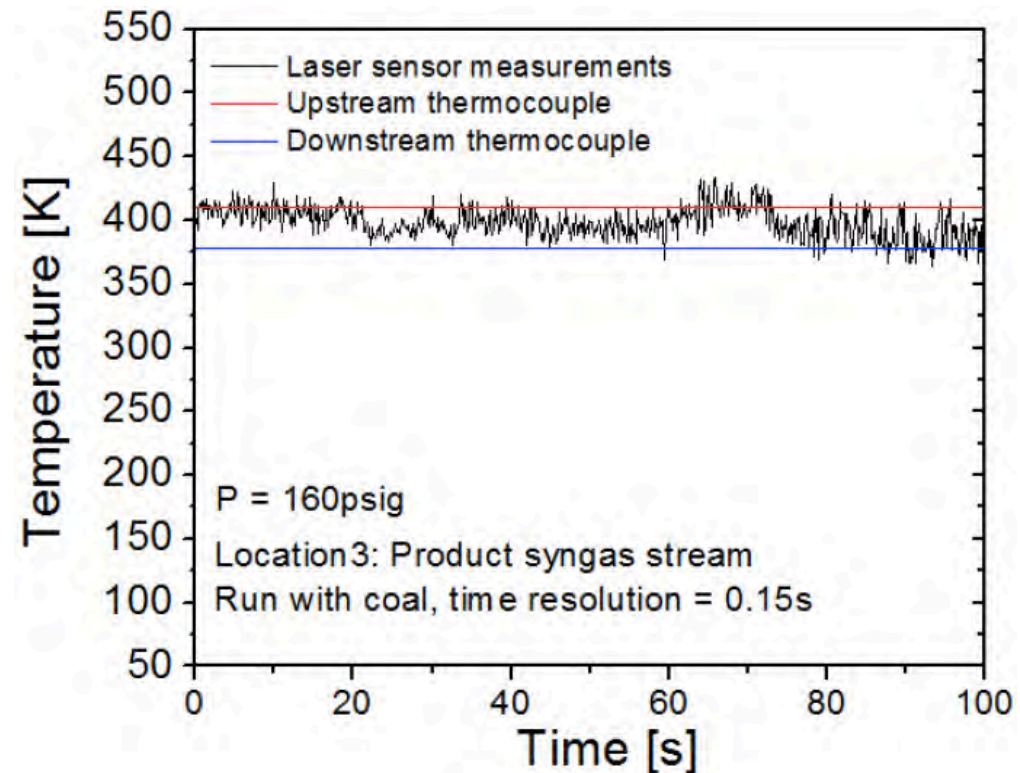


# TDL Sensor Results at Position 3

## Laser Transmission vs. Pressure

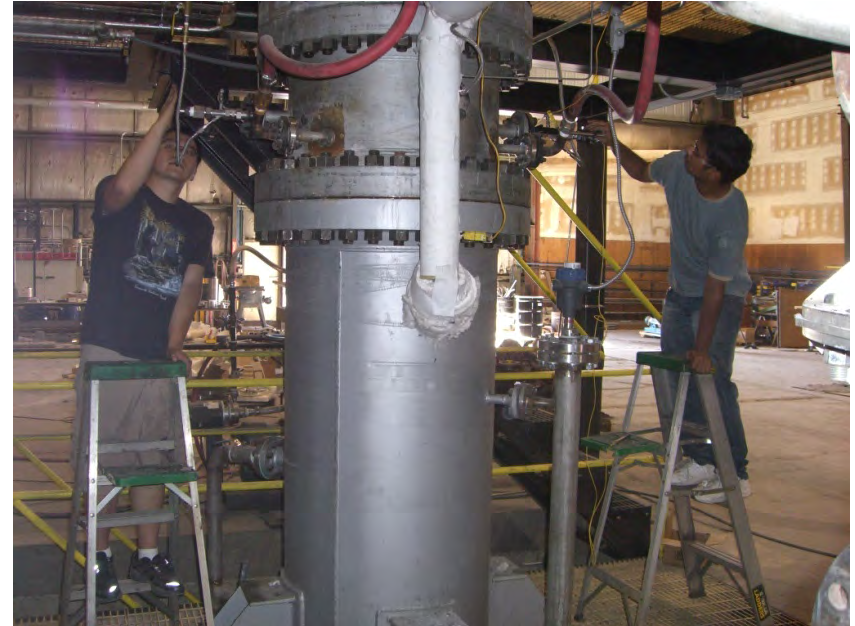
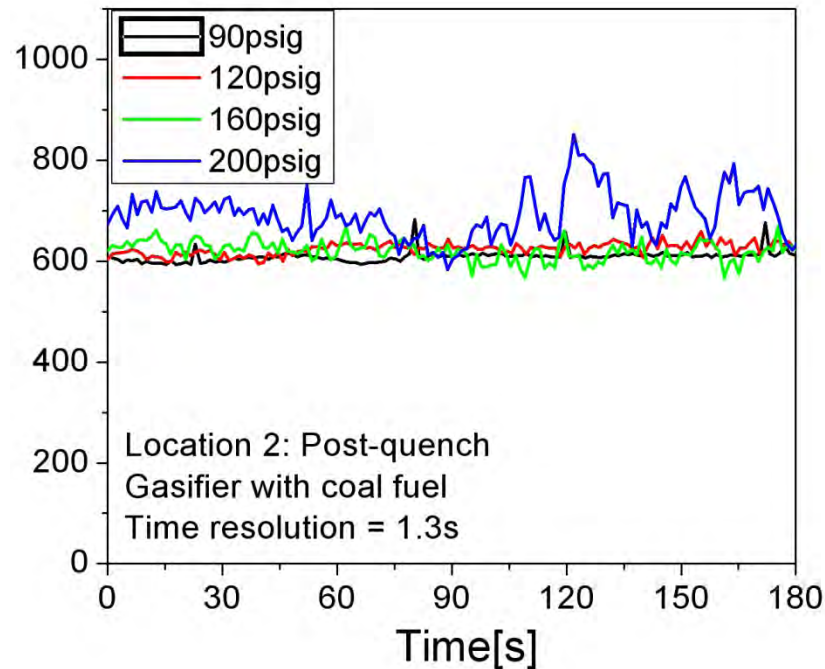


## Measured Temperature at 160 psi





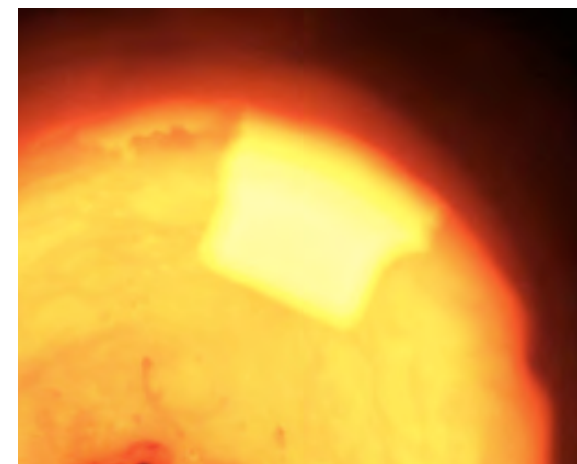
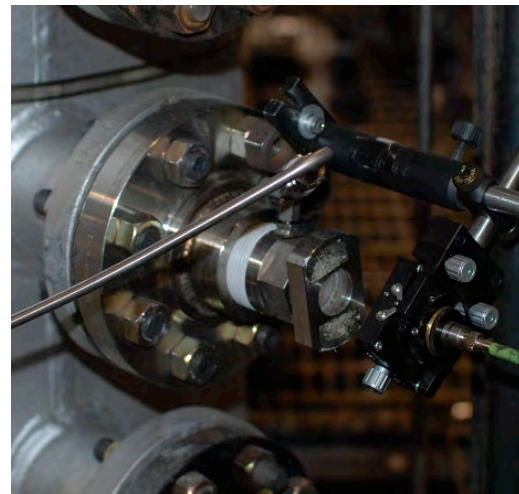
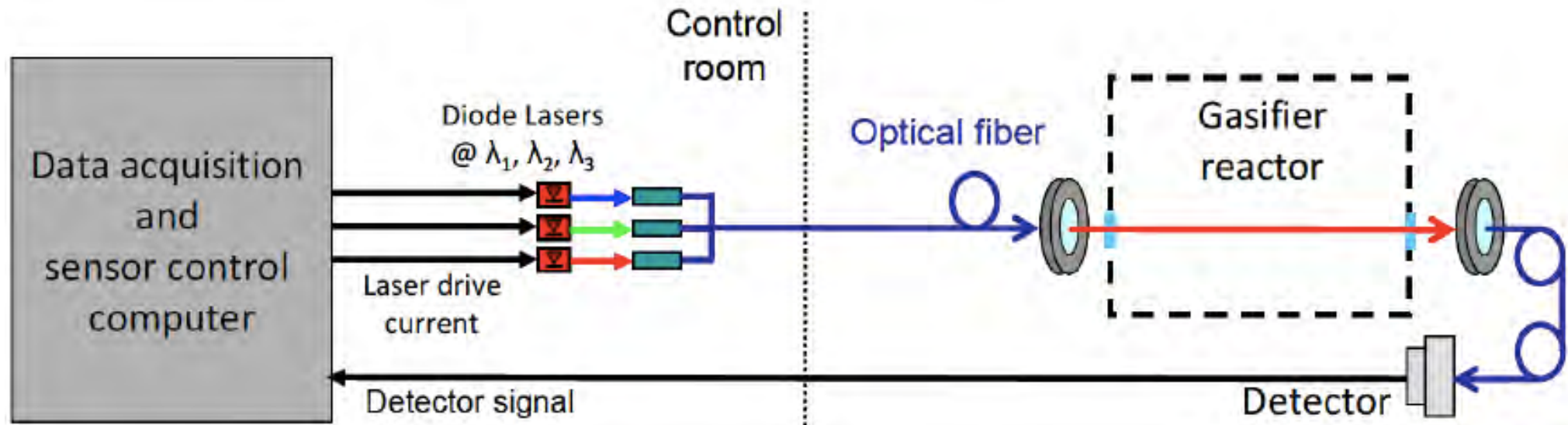
# TDL Sensing at Position 2



- High SNR, time-resolved measurements of T
- Normalized WMS accounts for varying transmission
- Measured T at reactor pressures of 90, 120 and 160psig stable
- Measured T at 200 psig identifies potential spray splashback instabilities



# TDL-Based Measurements within Reactor “Core” (Position 1)



# Validation Data Summary

## Conditions

- To 500 kWth
  - 1.5 ton/day coal
- 440 psia (30 atm) pressure
  - Typically operate at psia
- Temp to 3100°F (1700°C)
  - Typically 2400-2600°F
- Various fuels
  - Pittsburgh #8
  - Illinois #6
  - Utah Sufco
  - Texas Lignite
  - Petcoke

## Measurements

- Wall temperature
  - 5 positions
- Syngas composition
  - Post-quench
  - Pre-quench
- Reactor temperature
  - Integrated TDL-based
- Internal gas composition
  - Extractive sampling
  - Integrated TDL-based
- Internal condensed-phase
  - Extractive sampling



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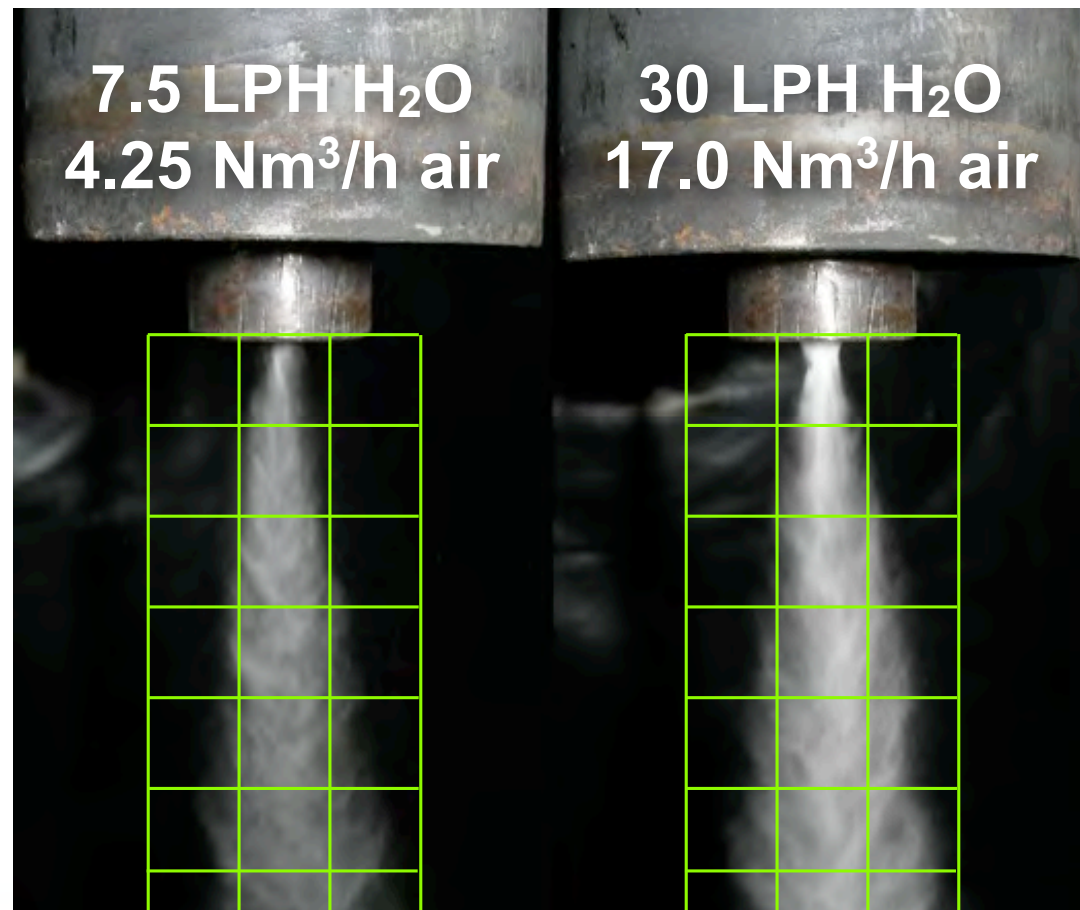
# Injector Cold Flow Test System

- Identification of injector performance
  - Uniformity
  - Spray angle
  - Droplet size
- Full scale model
  - Uses same injector as actual reactor
  - Air instead of oxygen
  - Water instead of slurry
- Pressurized system (to 5 bar) under development
- Analytical methods under development



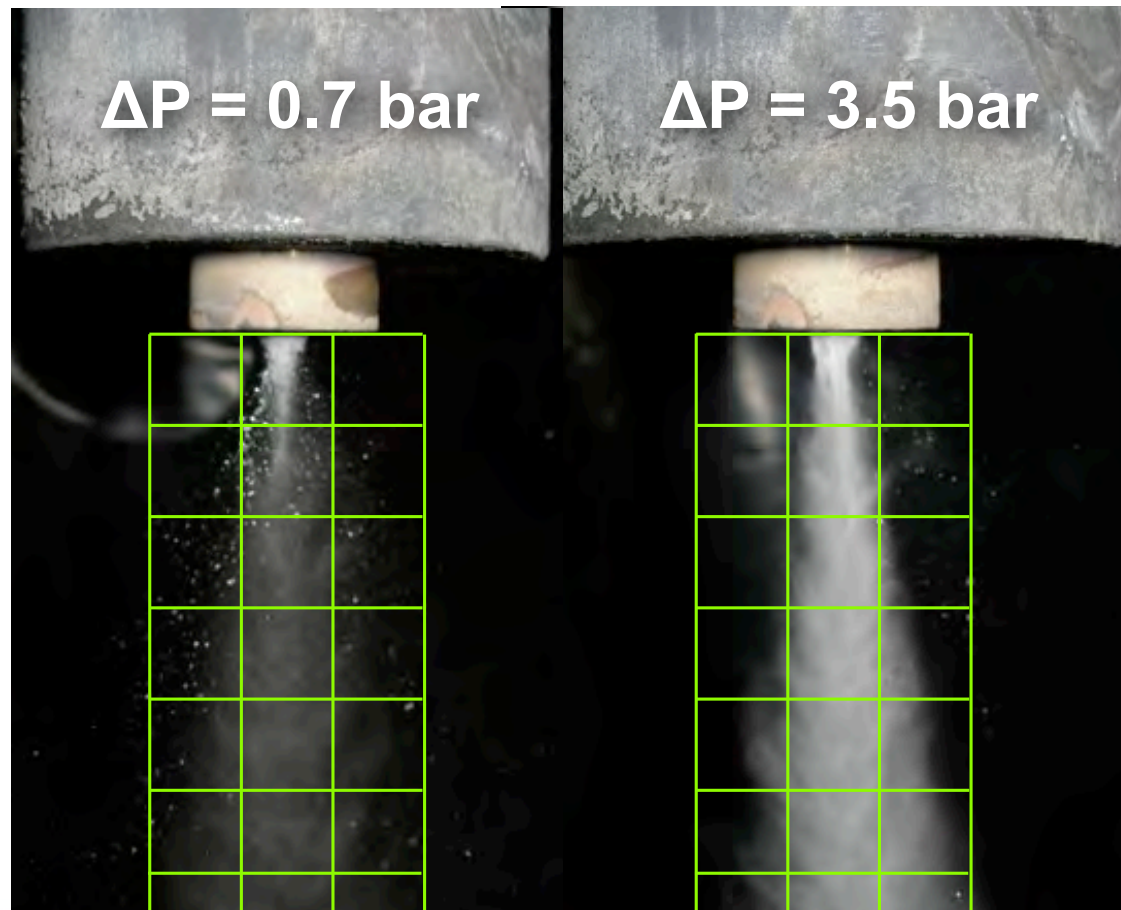
# Flow Rate

*Flow rates of air and water adjusted simultaneously to maintain air/water ratio  
Air pressure drop 2.8 bar  
45 degree nozzle*



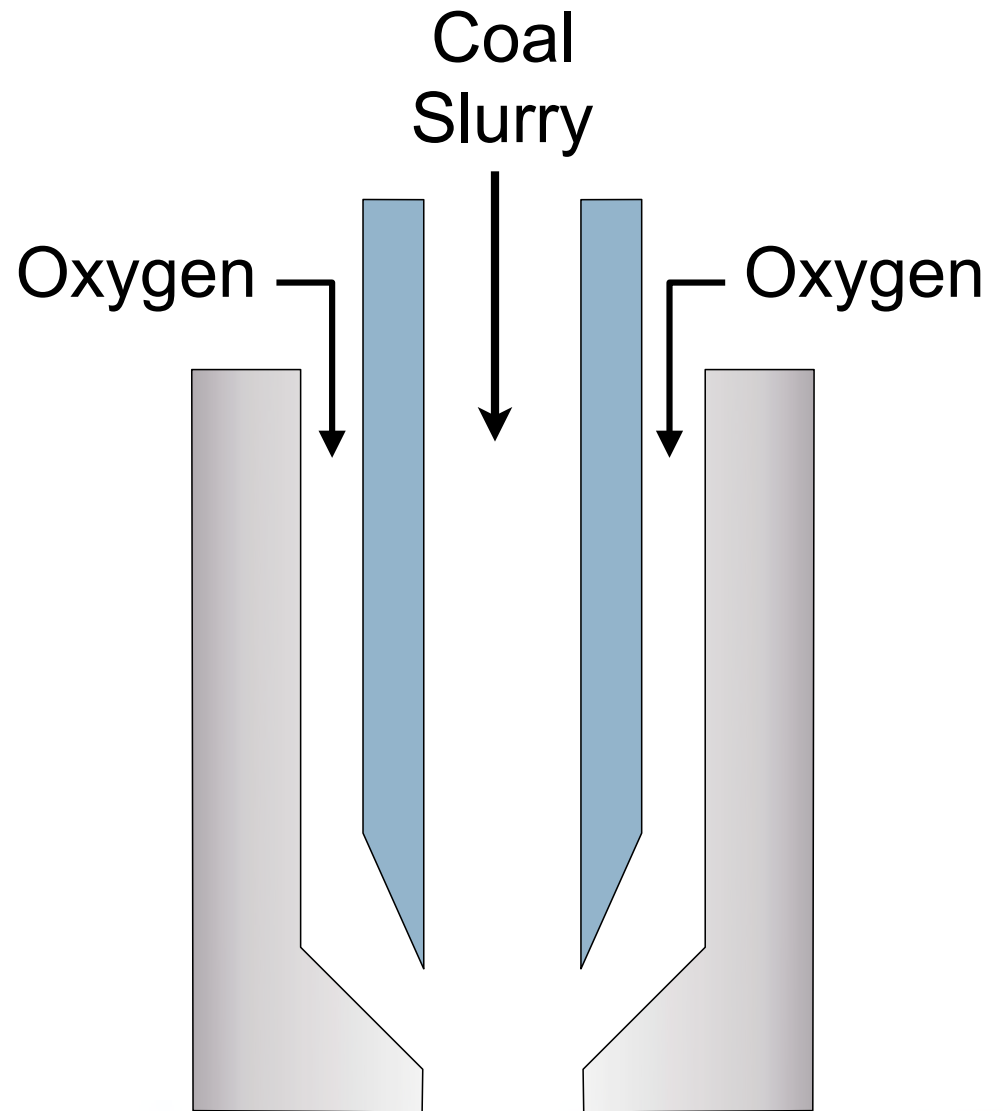
# Pressure Drop

*Both cases have 30 LPH water feed, 17 Nm<sup>3</sup>/h air feed  
65 degree nozzle*



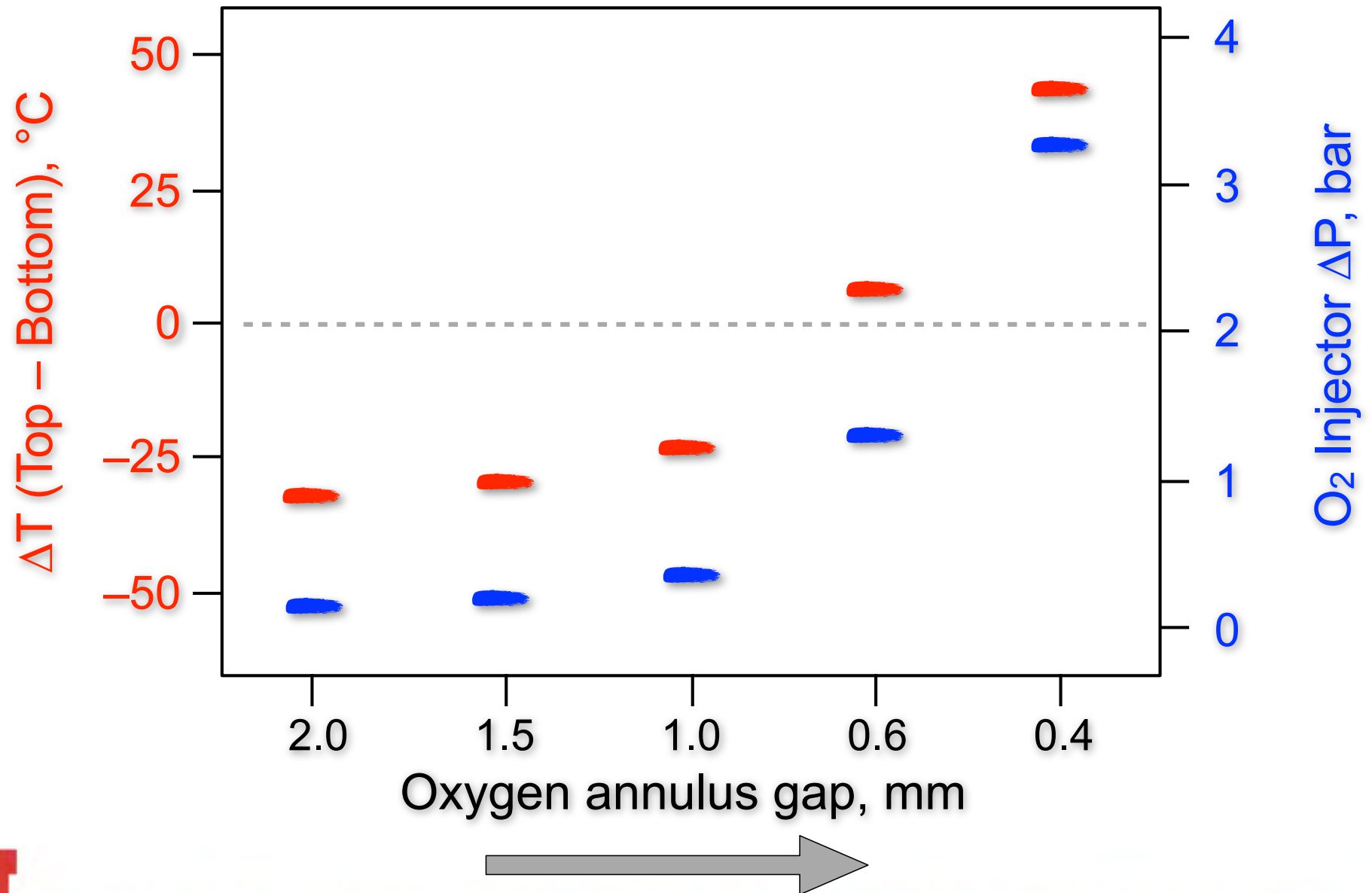


# Adjustable Injector Tip



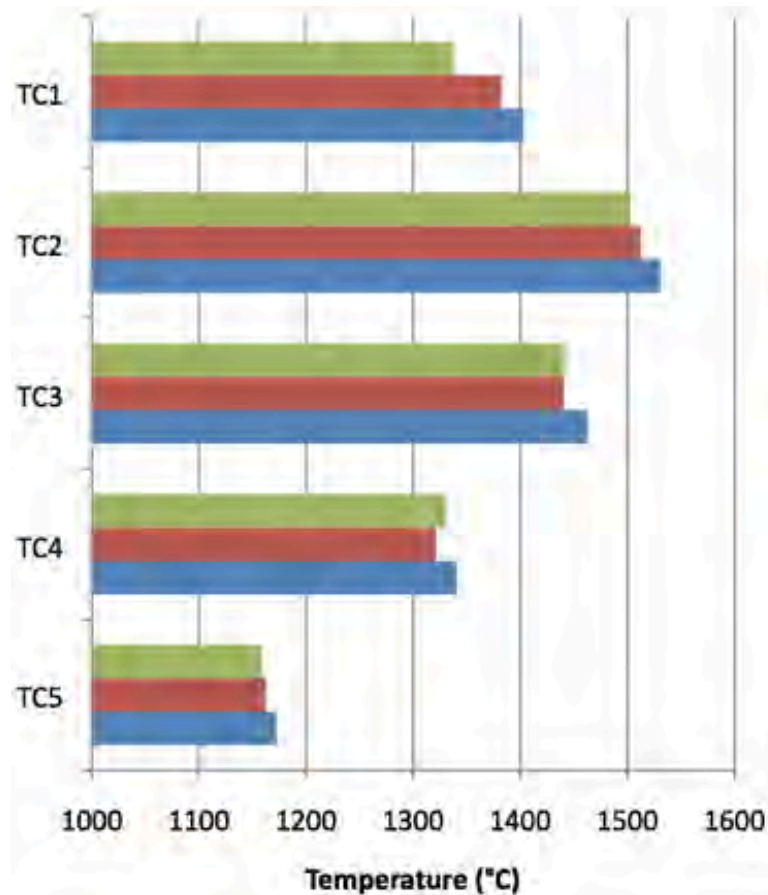


# Performance vs. Injector Gap

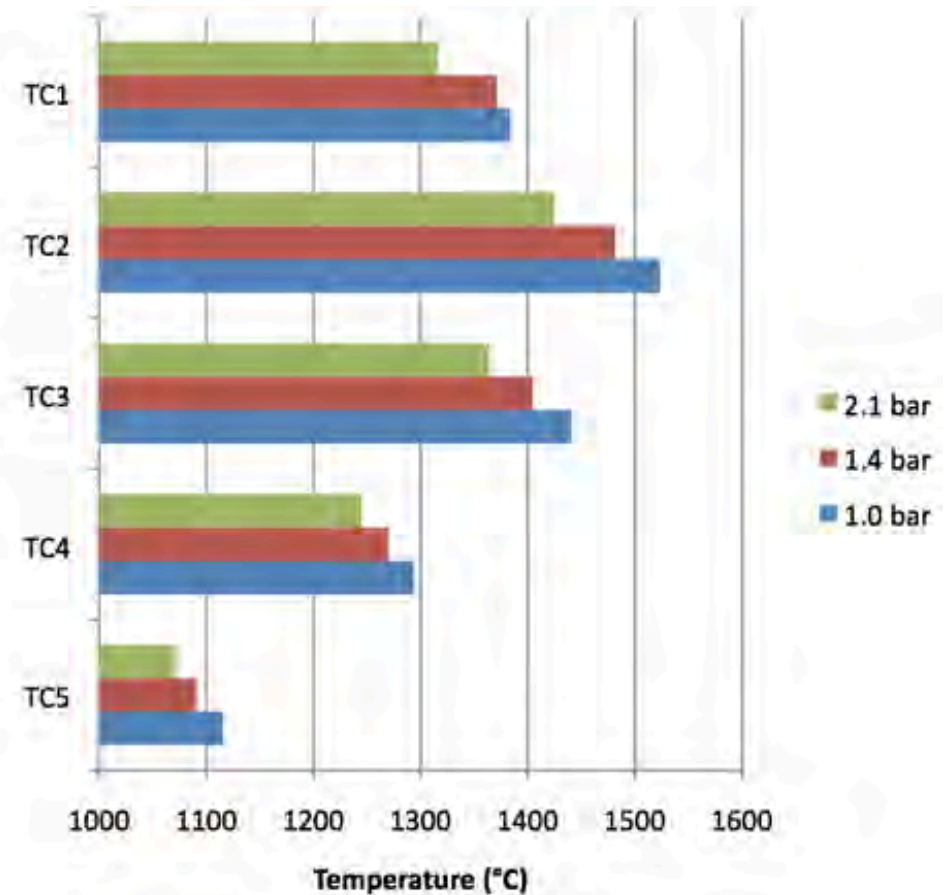


# Temperature Profile

45° nozzle angle (Day 1)

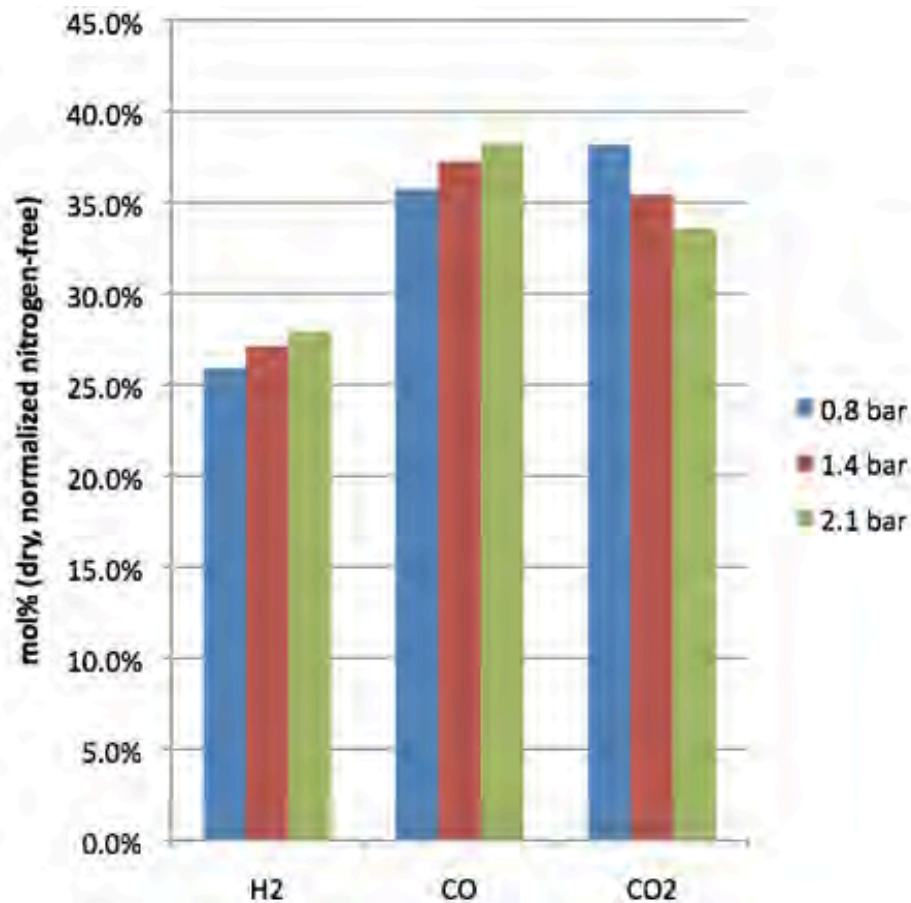


65° nozzle angle (Day 2)

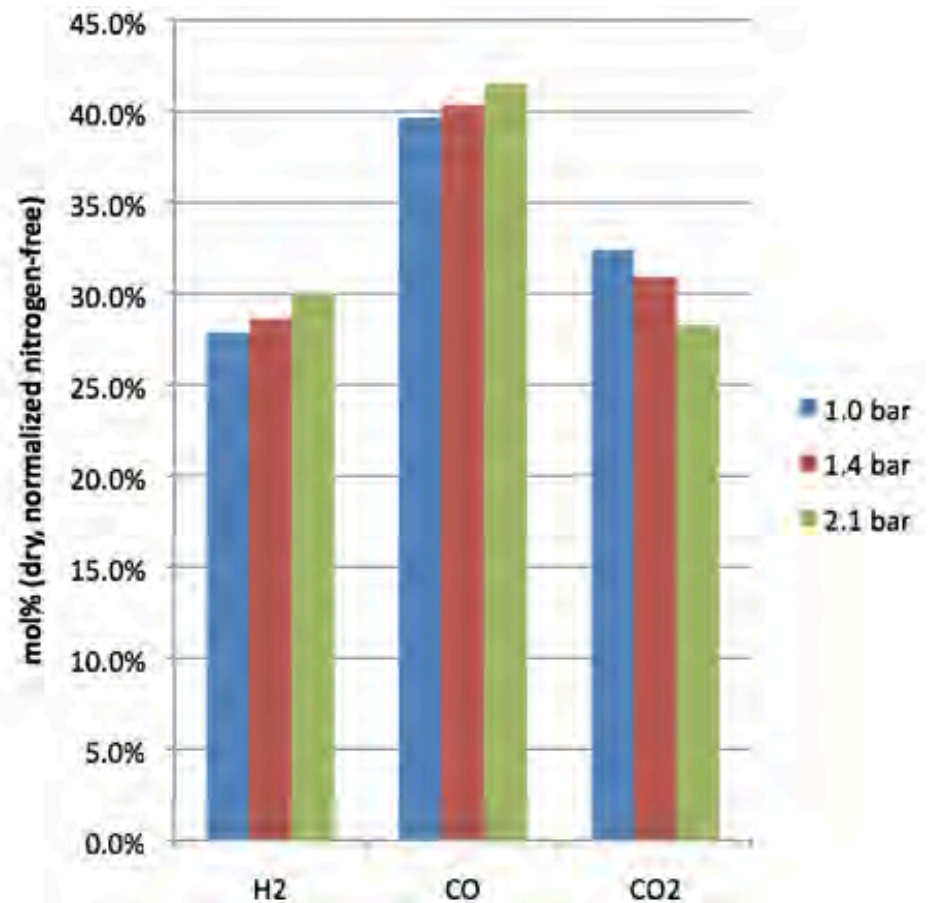


# Syngas Composition

**45° nozzle angle (Day 1)**



**65° nozzle angle (Day 2)**



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# Uncertainty Considerations

- **Temperatures:** Thermocouple junction located within wall, approx. 0.5 inch from refractory face, to extend thermocouple life
- **Gas composition:** Cooling within extractive probe may affect gas composition due to:
  - Changes in gas equilibrium composition at lower temperatures
  - Absorption of minor constituents (sulfur compounds, ammonia) by condensed water
  - Condensation of e.g., polyaromatic hydrocarbons as gas is cooled



# Uncertainty Considerations (2)

- **Condensed-Phase Material:** Difficult to obtain instantaneous compositions. Must be aggregate over time.
- **All Data:** Fluctuations on various time scales need to be quantified
  - 2 seconds
  - 20 minutes
  - Day-to-day



# Conclusions

- Acquisition of data within reaction zone of pressurized gasifier very challenging
- Gasifier performance strongly tied to injector design and efficiency of fuel distribution
- Optical techniques offer unique opportunity for real-time non-invasive sampling
- Quantification of data variation and associated uncertainty is important if data is to be used for validation of simulations





# Acknowledgements

- U.S. Department of Energy
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